

Amendments to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Canceled)
2. (Previously presented) The process according to claim 24, wherein the oxygenates and unsaturates are selected from the group consisting of normal alcohols, mono-olefins, and mixtures thereof.
3. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least 0.5 wt% normal alcohols as oxygenates.
4. (Original) The process of claim 3, wherein the normal alcohols boil in the range of from about 50°C to about 350°C.
- 5 – 6. (Canceled)
7. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 5.0 wt % mono-olefins.
8. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 15.0 wt % mono-olefins.
9. (Original) The process of claim 2, wherein the hydrocarbon stream comprises at least about 25.0 wt % mono-olefins.
10. (Original) The process of claim 9, wherein the mono-olefins boil in the range of from about -105 to 350°C.

11. (Previously presented) The process of claim 24, wherein the Fischer-Tropsch hydrocarbon stream is a low-boiling fraction in a range from about -65°C to about 350°C.
- 12 – 15. (Canceled)
16. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is from a hydrogen production unit.
17. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is recycled from a hydroprocessing operation.
18. (Previously presented) The process of claim 24, wherein the first hydrogen-containing gas is syngas.
- 19 – 23. (Canceled)
24. (Currently Amended) A process for hydroconversion of a Fischer-Tropsch hydrocarbon stream including oxygenates and hydrocarbon unsaturates with reduction in formation of heavy molecular weight products during heating comprising at least one preheating step prior to a heating step for achieving hydroconversion reaction temperature, the process comprising:
 - a) adding a first hydrogen-containing gas to the hydrocarbon stream prior to the at least one preheating step and not under hydroconversion conditions, wherein the first hydrogen-containing gas is added in an amount less than about 100 SCFB and wherein the first hydrogen-containing gas is sufficient to reduce the amount of heavy molecular weight products formed during the preheating as compared to a heated hydrocarbon stream without added hydrogen, to form a mixed stream;

- b) preheating the mixed stream;
- c) adding a second hydrogen-containing gas to the preheated mixed stream sufficient to effect hydroconversion of the mixed stream, to form a hydroconversion feed stream;
- d) heating the hydroconversion feed stream to reaction temperature; and
- e) hydroconverting the hydroconversion feed stream.

25 – 26. (Canceled)

27. (Original) The process of claim 26, wherein the first hydrogen-containing gas is added in an amount less than about 50 SCFB.

28. (Original) The process of claim 24, wherein the second hydrogen-containing gas is added in an amount more than 750 SCFB.

29. (Previously presented) The process of claim 24, wherein the mixed stream is preheated to a temperature in the range of from about 120°C to about 400°C.

30. (Previously presented) The process of claim 24, wherein the mixed stream is preheated to a temperature in the range of from about 250°C to about 400°C.